

Gas Lift Workshop Houston – USA 4-8 February 2008

API RP 11v11
Recommended Practice for
The Use of Dynamic Simulation
of Gas Lift Wells and Systems

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#### CONTENT

- This presentation describes dynamic simulation and its current applications for gas-lift wells and systems.
- It gives an overview of the plans for a new API Recommended Practice for Dynamic Simulation of Gas-Lift Wells and Systems: API RP 11V11.

### API 111V Gas-Liff: Task Group



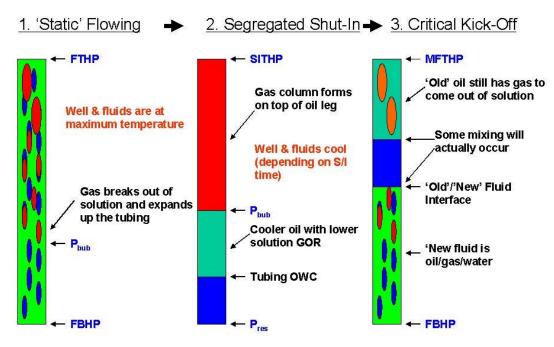
APR-RP-11

Although our primary focus is currently on gas-lift, we intend to address a broad range of artificial lift systems and topics

#### **NODAL® vs. DYNAMIC SIMULATION**

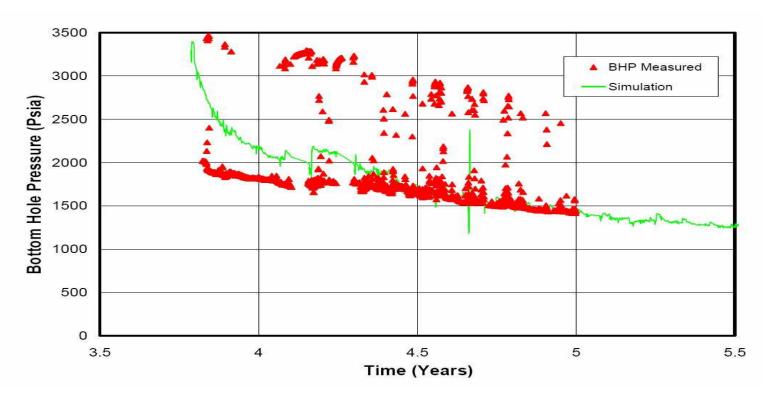
The weak points of NODAL S.S. analysis comparing with dynamic (transient) simulation are:

- Unable to predict severe slugging introduced by riser / flowline or HL / ML / sinusoidal wellbores
- Unable to perform instability analysis
- Unable to performance gas-lift unloading analysis
- Unable to predict dynamic behaviour of plunger lift
- Unable to look at gas/condensate gas well liquid load-up issues
- Unable to performance flow assurance study, e.g., start-up / shutdown, corrosion / chemical injection



#### **NODAL® vs. DYNAMIC SIMULATION**

- Steady state simulation tools (Prosper, etc.) are inappropriate for dynamic (transient, change with time) multi-phase flow in wellbores.
- An example of discrepancy btw. S.S. model and measured results for a CVX gas-condensate well (Britannia, North Sea).

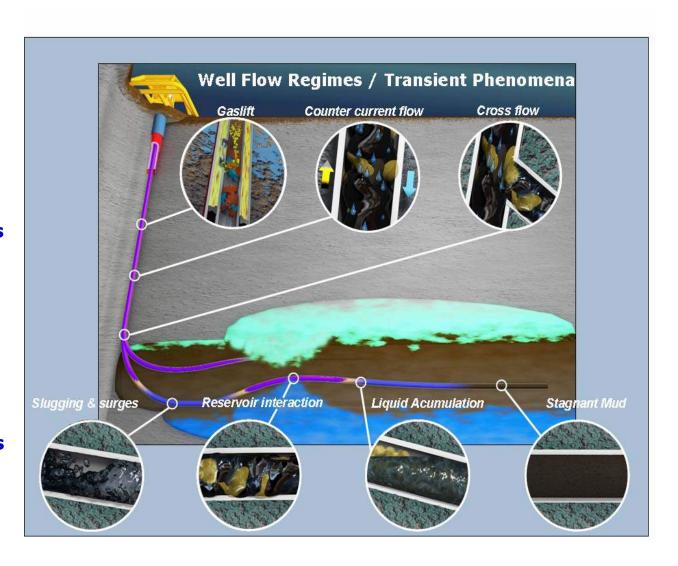


### **DYNAMIC SIMULATION**

- Dynamic simulation can be used at any stage of a field's life cycle to build a virtual model of a well and/or production system.
- It can help to understand transient well behaviour and determine the optimum process to eliminate or minimize instability problems.
- It can be used to analyse "what if" scenarios and predict results.
- It does not replace NODAL® analysis but fills gaps where steady-sate analysis techniques cannot provide adequate solutions.

# **Dynamic Simulation Recommended Areas of Use**

- Gas-lift unloading
  / plunger lift
- Instablility /
  Severe Slugging
- Gas-lift design and optimisation
- Cross-flow analysis
- Gas well Liquid load-up
- Well Clean-up / start-up
- Well Testing:
  Wellbore Storage
  effects /
  Segregation effects
- Wellbore thermal calculations
  - Flow Assurance



### DYNAMIC GAS LIFT APPLICATIONS

- Continuous gas-lift / Gas-lift valve performance
- Intermittent gas-lift
- Gas-assisted plunger lift
- Dual gas-lift
- Single-point gas-lift
- "Auto" gas-lift (gas from one zone is used lift other zones)
- Riser gas-lift
- Gas-lift for gas well deliquification
- Gas-lift unloading
- Kick-off of gas-lift wells
- Use of gas-lift for wellbore clean-up
- Gas-lift system distribution with various types of system configurations
- Use of un-dehydrated gas
- Use of non-hydrocarbon gases such as CO2 and N2.

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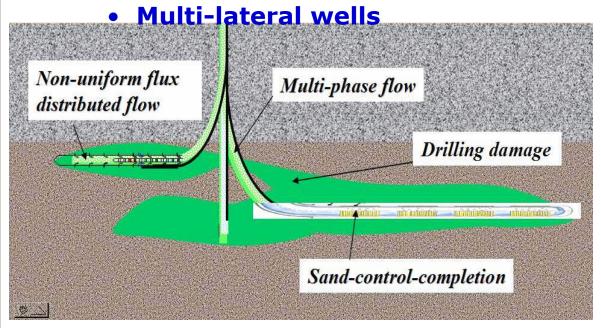
#### DYNAMIC SIMULATION for WELL DESIGN

#### Well design:

Understand effects of well design & associated dynamic

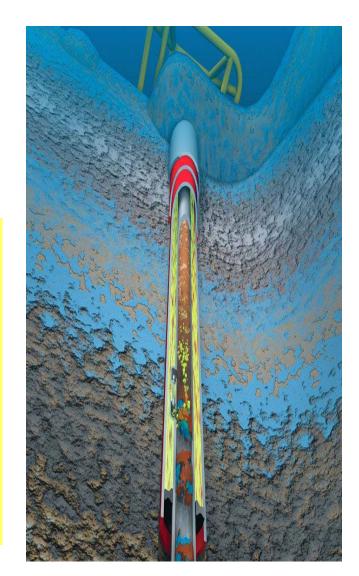
effects on well operations, including:

- Vertical wells
- Horizontal / Sinusoidal wells



## Example 1: Dynamic Simulation for Dry-Tree Gas-Lift (injection at the mud line)

- An example for subsea deepwater G-L, where transient issues relates to flow assurance, complex wellbore. Long flowlines / risers play significant roll in G-L system design and optimization.
  - •10,000' vert. well (5 ½" tb x 9 5/8" cs) from reservoir to riser base (mud line), drill water fills well annulus.
  - •5,000' riser (1.5" insulate layer) to dry tree.
  - •Gas injected downward from surface (125F) to the 9 5/8" riser annulus. Riser-base is a merge node where well & annulus converge into the riser.

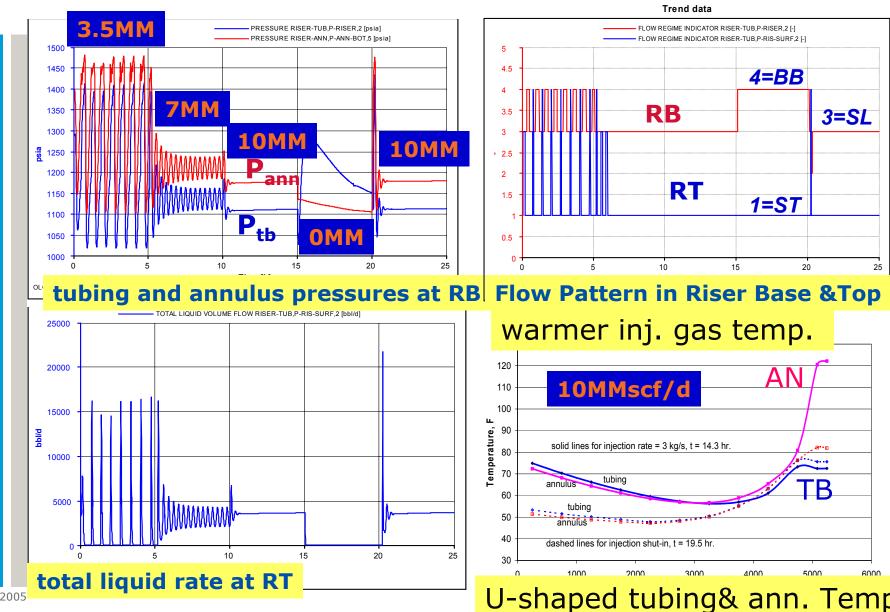


### Example 1: Dynamic Simulation for Dry-Tree Gas-Lift (injection at the mud line) (courtesy to Lee Norris)

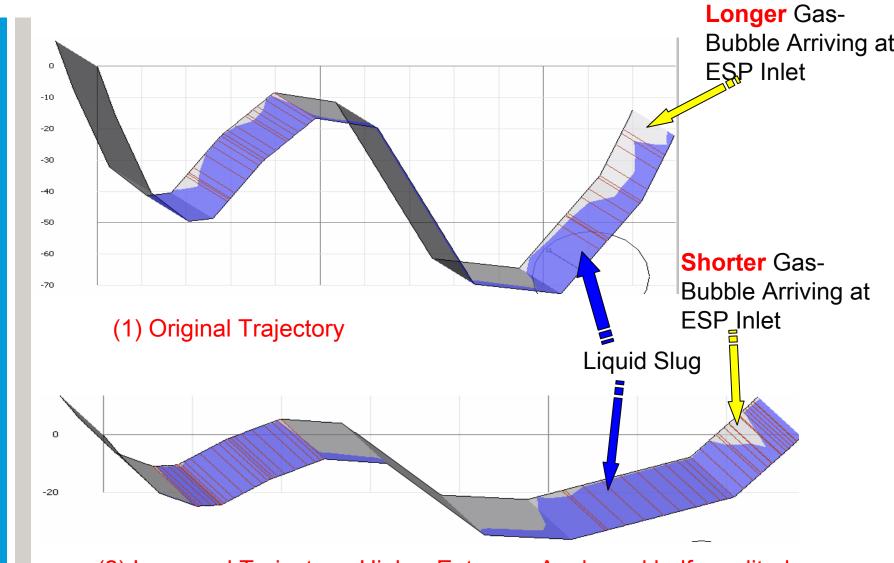
•Simulate unstable and stable production by injecting different quantities of gas, U-shaped temperature profiles due to counter-current flow and heat exchange through annulus and riser, the effect of downtime of injection operation and the restart of gas-lift.

- •0 ~ 5 hr.: 3.5 MMscf/d gas injection
- •5 ~ 10 hr.: 7.0 MMscf/d gas injection
- •10 ~ 15 hr.: 10.5 MMscf/d gas injection
- •15 ~ 20 hr.: gas injection stopped
- •20 ~ 25 hr.: resume 10.5 MMscf/d gas injection
- •Sea Water@ riser top=76 F, Sea water@ mud-line=43 F

# Example 1: Dynamic Simulation for Dry-Tree Gas-Lift (injection at the mud line)

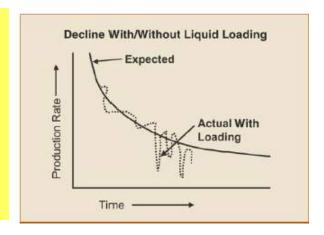


## **Application Example 2: CVX Sinusoidal Wells Trajectory Design to Reduce Instability**

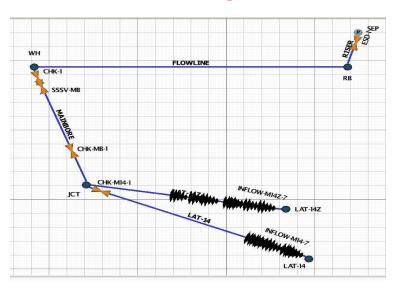


### Application Example 3: CVX Dual Laterals Liquid Load-up Study

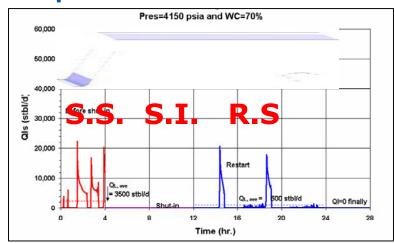
A dual-lateral well was completed in a cvx subsea condensate field with high peak rate (77 MMscf/d and 6300 stbo/d). Within one year, the production significantly declined with high water-cut (WC=90%).



• After a shut-in the well came on-line at a much reduced rate and over a period of 3 days stopped producing.

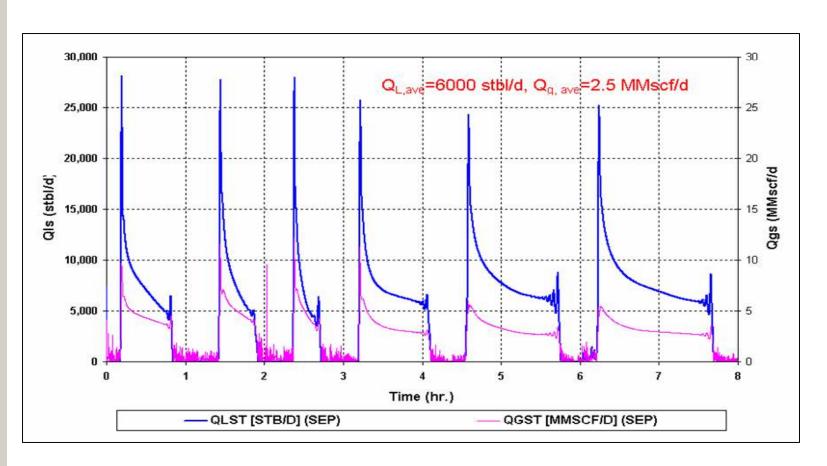






### **Application Example 3: CVX Dual Laterals Liquid Load-up Study**

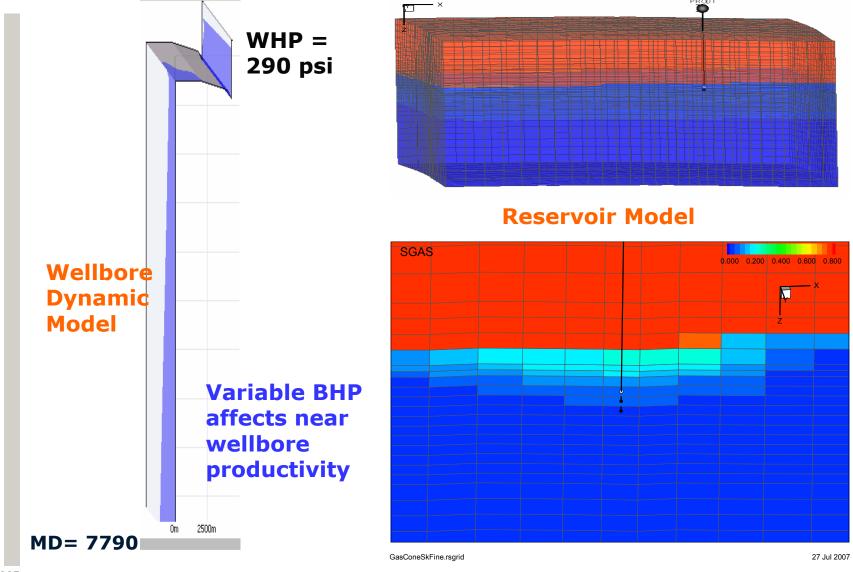
#### Flow Rate at Separator, Gas-Lift has been stopped



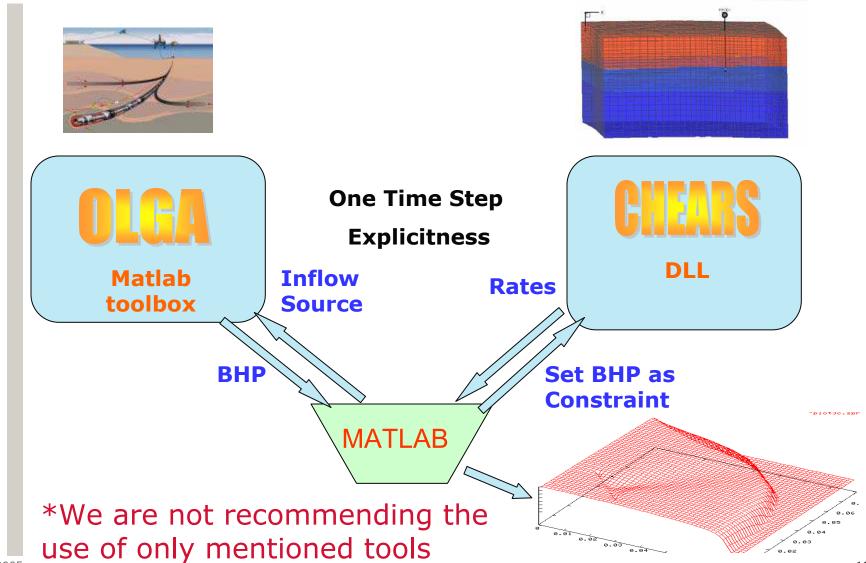
Well becomes intermittent after gas-lift stop

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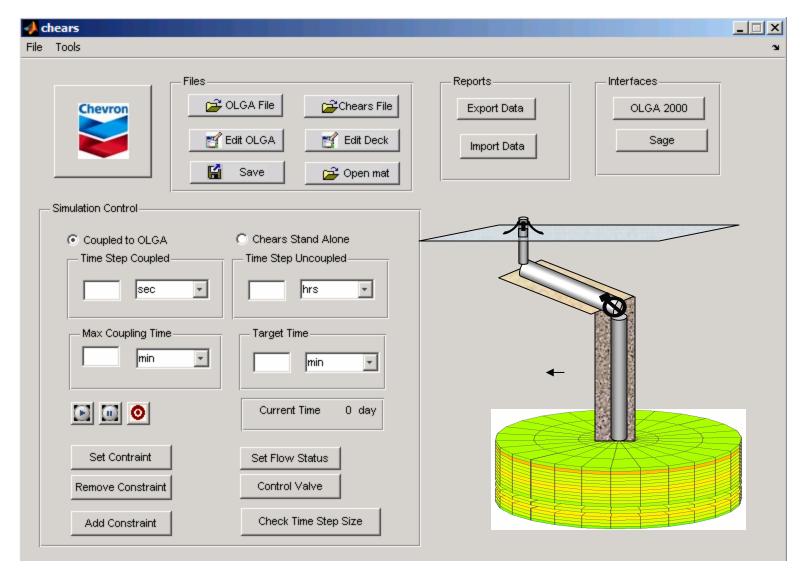
# **Application Example 4: Integrated Wellbore-Reservoir Dynamic Simulation**



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# **Application Example 4: Integrated Wellbore-Reservoir Dynamic Simulation**



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### **DYNAMIC SIMULATION PRACTICES**

- Currently, there are no industry-accepted recommended practices for the application of dynamic simulation for gas-lift.
- The industry recognizes the needs for a API RP for Dynamic Simulation of Gas-Lift Wells and Systems: API RP 11V11.

### **API RP 11v11 TEAM MEMBERS**

- Following the API Standards Development procedures, we formed a working team committee to develop written recommendations and guidelines for dynamic simulation techniques.
- We would like to invite you to be a member of the committee and participate in shaping these global standards to contribute your experience and to represent your company.
- Our next meeting is scheduled to be held on Friday 8/02/08

# API RP 11v11 TASK GROUP MEMBERS

#### 16 members representing 14 companies and one university

Juan Mantecon, SPT Group - Chairperson **Cleon Dunham, Oilfield Automation - Secretary** Adam Ballard, BP Arne Valle, StatoilHydro **Boots Rouen, Schlumberger** Dan Dees, AppSmiths Fernado Ascencio Candejas, PEMEX Dr. Fernando Samaniego, UNAM (Mexico Autonomous Nacional **University**) Galileu Paulo Henke A. Oliveira, Petrobras **Greg Stephenson**, eP-Solutions Kallal Arunachalam, ConocoPhillips Ken Decker, Decker Technology Knud Lunde, StatoilHydro Murat Kerem, Shell **Shanhong Song, Chevron** Yula Tang, Chevron