



# Whatever Happened to Pump Stroke Optimization?

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***ENCLINE***



# History of Pump Stroke Optimization

- ▶ Concept and data from two pilot wells first presented to industry at ALRDC Sucker Rod Pumping Workshop in September 2015
- ▶ Case Study of 20 Well Eagle Ford pilot presented at Southwestern Petroleum Short Course in April 2016, and in peer reviewed SPE Paper 181228-PA
- ▶ Four well Bakken pilot presented in September 2016 at ALRDC Sucker Rod Pumping Workshop



# What is Pump Stroke Optimization?

- ▶ Part 1: For wells with excess pump capacity, preferentially slowing pumping speed on downstroke
  - ▶ Results in less slippage and better pump fillage
  - ▶ Referred to as **Slow Downstroke Mode** or SDSM
- ▶ Part 2: Address the problem of wave and slug flow in horizontal wells that mislead RPC's into cycling between max and min speeds
  - ▶ Results in poor pump fillage and rod buckling
  - ▶ Requires setting max pumping speed near average



# PSO Part 1: “Slow Downstroke Mode”

## Two ways to run at 3 SPM

- ▶ Old School Method for 3 SPM
  - ▶ Total stroke duration is 20 seconds
  - ▶ Upstroke duration is 10 seconds, as is downstroke
- ▶ Slow Downstroke Mode (SDSM)
  - ▶ 6 SPM on upstroke, a 5 second duration
  - ▶ 2 SPM on downstroke, a 15 second duration
  - ▶ Total stroke duration still 20 seconds but upstroke duration only 25% of each stroke, not 50% (5/20 instead of 10/20)

# SDSM Example: Pumping at 3 SPM

Artificial Lift  
R&D Council



# Use of the Pump Slippage Equation to Design Pump Clearances (Rowlan, McCoy, Lea)

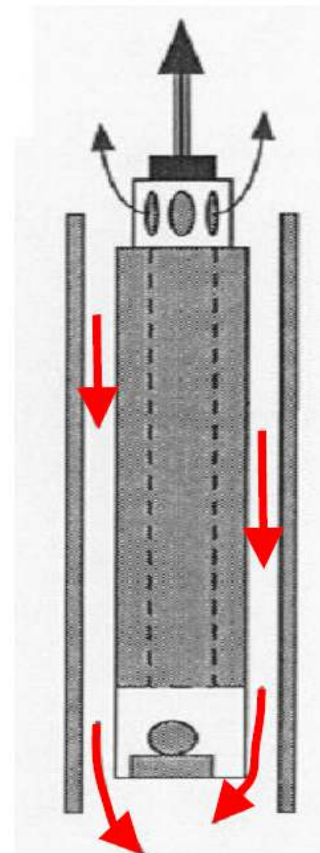
## Pump Slippage

- 1) Fluid that leaks back into pump between the Plunger OD and the Barrel ID
- 2) Leaks into the pump chamber between the standing valve and traveling valve
- 3) When traveling ball is on Seat.

**Pump Efficiency =**  
**BPD Tank / BPD Pump**

**Slippage % =**  
**Slippage BPD / BPD Pump**

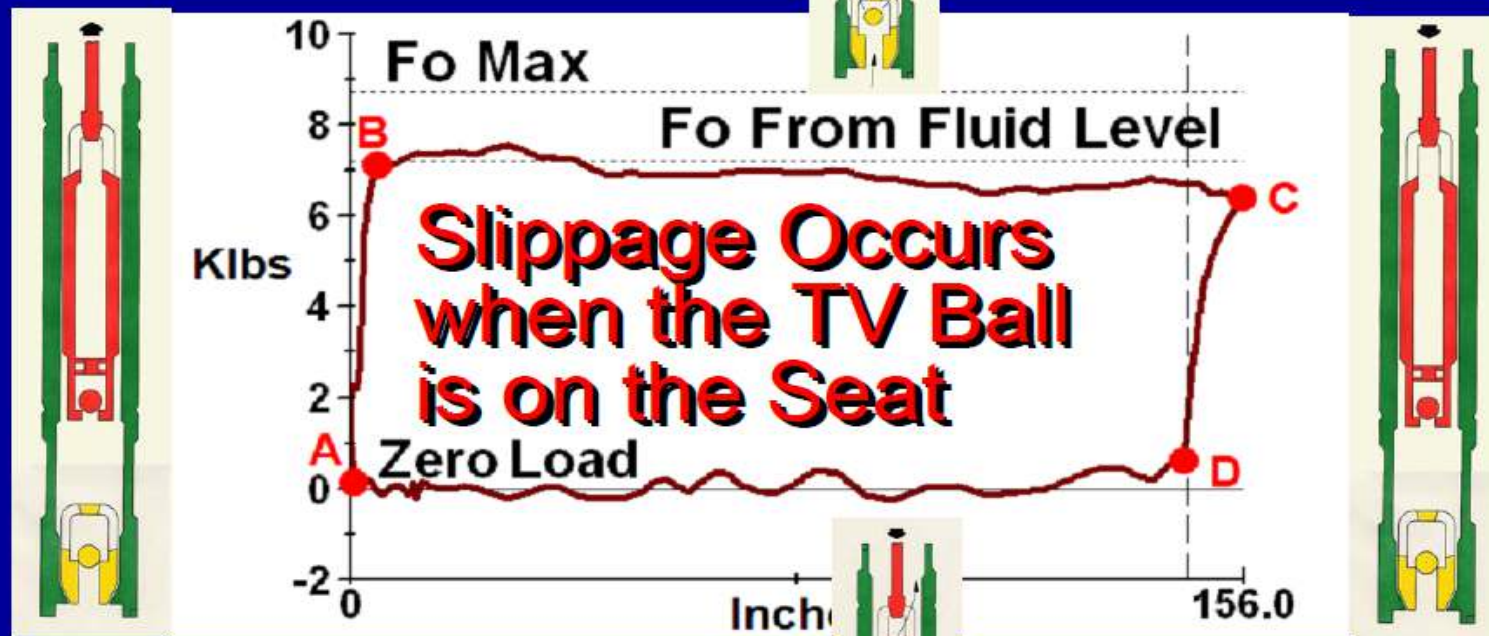
**BPD Tank = BPD Pump**  
**- Slippage**





1) Point A to B pressure acting on closed SV gradually transferred from tubing at point A to be fully carried by the Closed TV at point B.

2. Point B to C, plunger carries full differential pressure across Closed TV



4) Point D to A, TV open as fluid in the pump is displaced through the traveling valve on the down stroke

3) Point C to D pressure across closed TV gradually transferred from rods to be fully carried by the Closed SV at point D.

# Observations about Pump Slippage



- ▶ Pump Slippage during the Upstroke reduces system efficiency
  - ▶ Since standing valve is open, slippage replaces fluid that would normally enter pump
  - ▶ Less Time on Upstroke = Less pump slippage
- ▶ Pump slippage during the Downstroke does not impact system efficiency, but improves fillage
  - ▶ Since standing valve closed during downstroke, new well fluids not entering the pump anyway
  - ▶ Slippage fluids fill pump, opening travelling valve sooner
    - ▶ Pump fillage increased, reduced rod buckling



# From SPE 181228: Pump Slippage Equation Correction



- ▶ 2001 Thesis by Chambliss submitted to Texas Tech: “Plunger Leakage and Viscous Drag for Beam Pump Systems”
  - ▶ Pump slippage greater for alternative geometry pumping units that had unequal upstroke and downstroke travel time

$$B_{Adjusted} = \frac{Degrees_{UP}}{180} B_{Calculated}$$

- ▶ However, Chambliss did not consider variation in pumping speed induced travel time differences. A revised equation that considers both is presented:

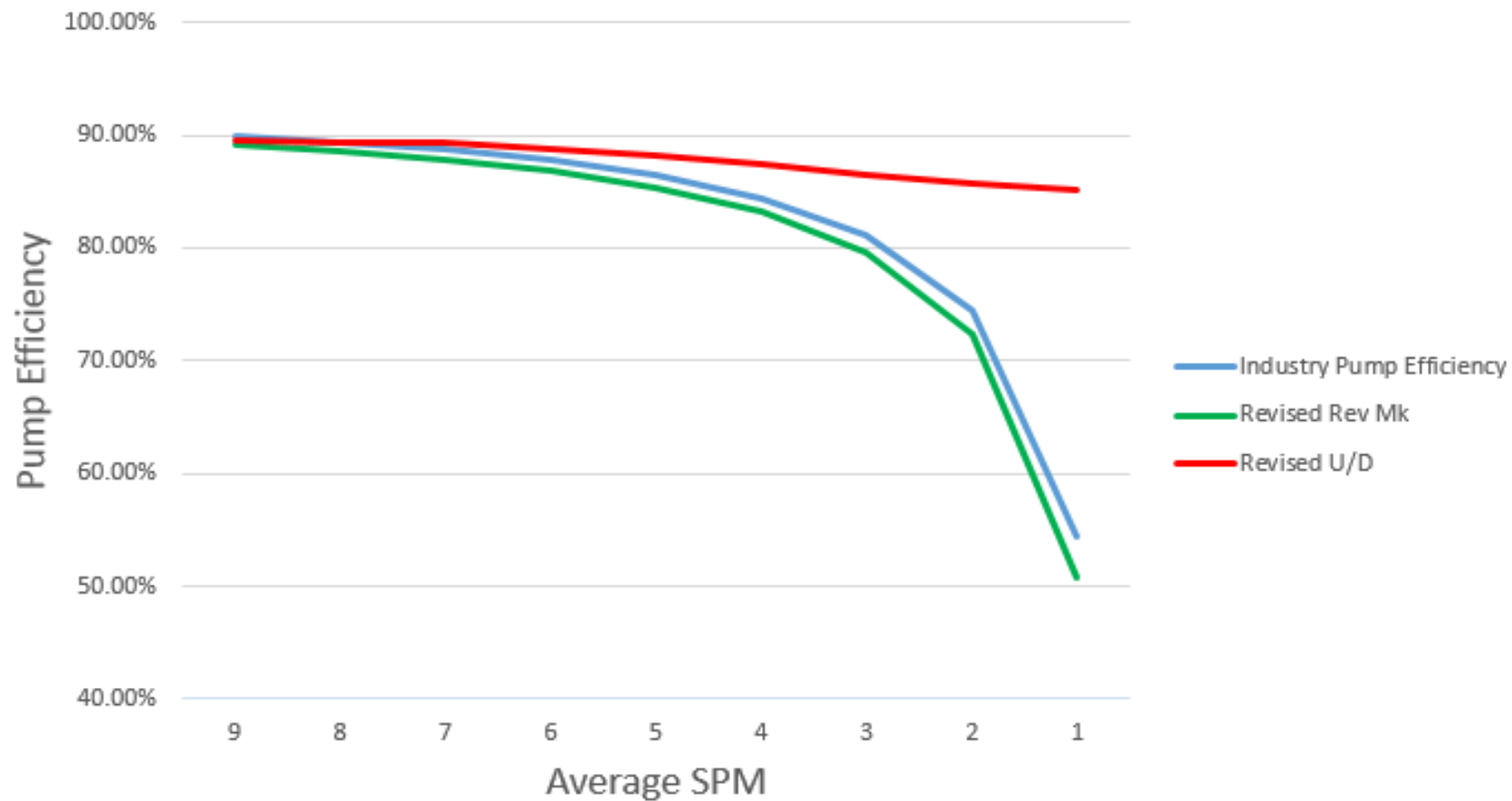
$$B_{Adjusted} = (2 \times T_{Upstroke} \times B_{Calculated}) / (T_{Downstroke} + T_{Upstroke})$$

# Patterson slippage formula modified for % Upstroke Duration

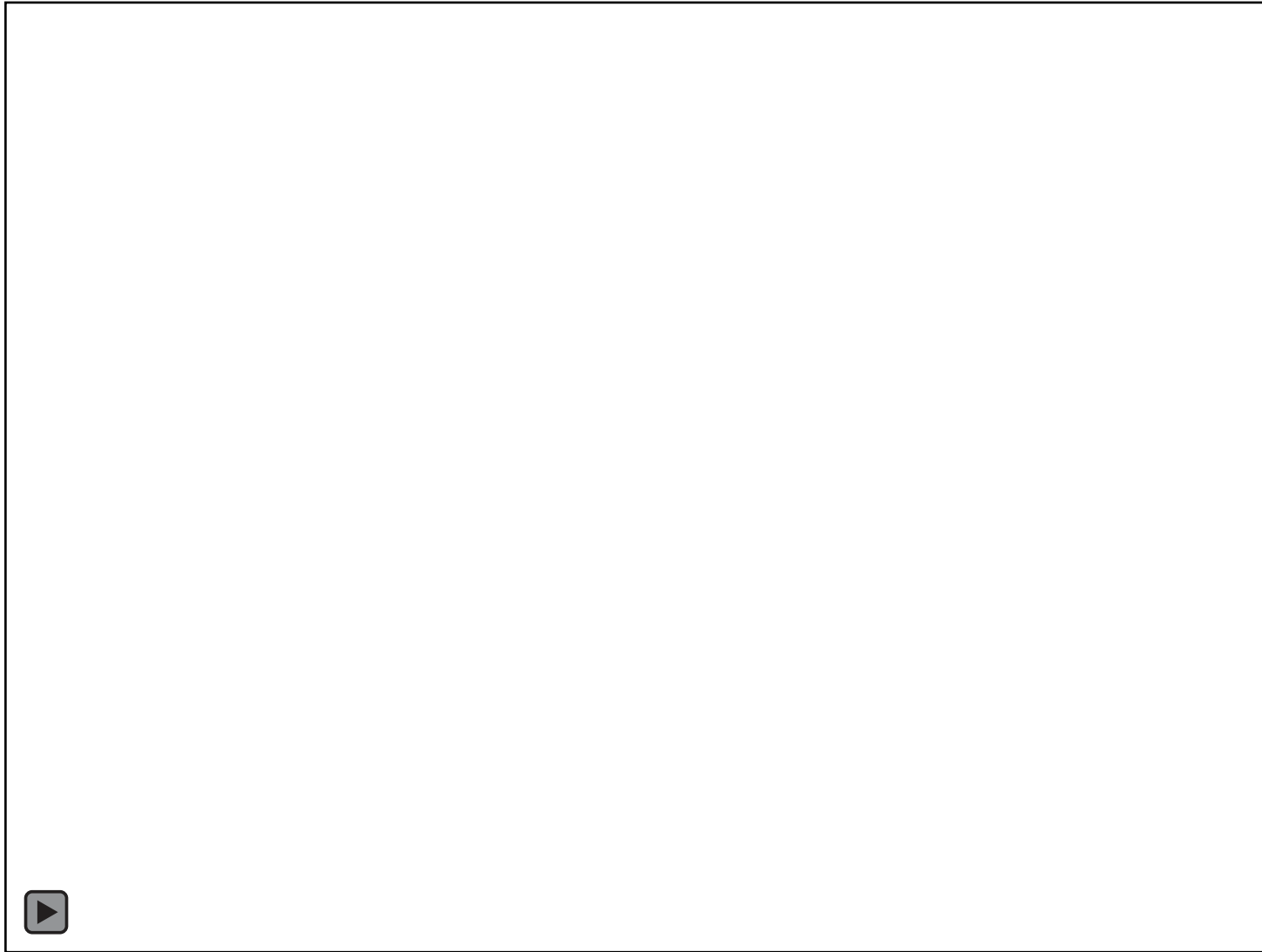


## Pump Efficiency Using Arco-HF-COP Base, Reverse Mark, U/D Speed Control

1.5" Pump at 10000 Feet with .006 clearance, 0.7 vis  
350 psi PIP, 6 foot plunger, 0.8 gravity fluid  
4 SPM Max SPM Differential, 4 sec Accel/Decel



# PSO Part Two: Setting Pumping Speeds





# How do operators address poor pump fillage due to horizontal well slugging?

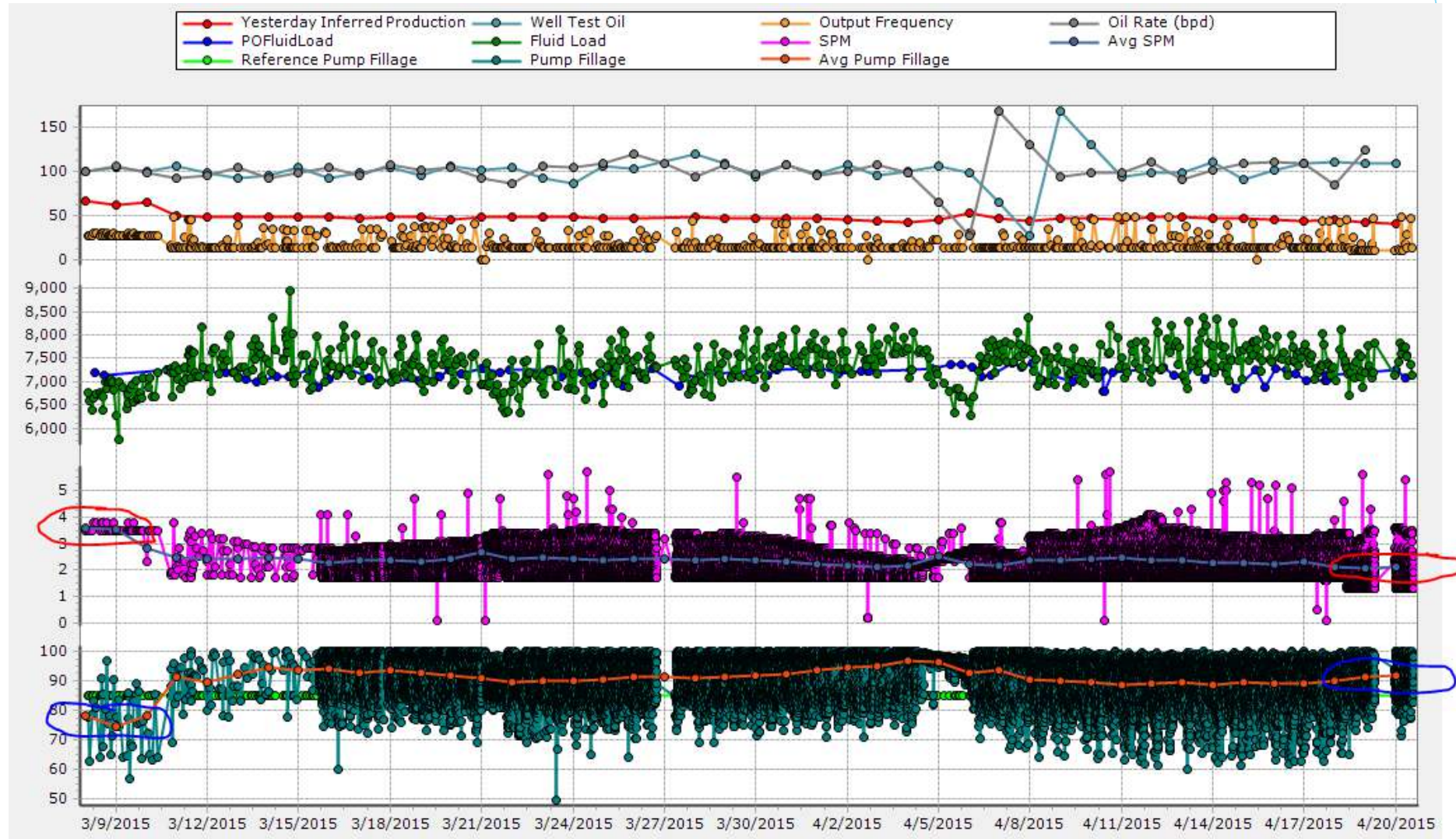
- ▶ By manually setting pumping speed
  - ▶ Limiting maximum pumping speed
  - ▶ Reducing the minimum pumping speed
- ▶ The current approach requires
  - ▶ Regular monitoring by personnel
  - ▶ Resetting pumping speeds as wells continue to deplete
- ▶ PSO Part 2 is autonomous setting of these speeds



# SDSM (PSO Part 1) decreases slippage and increases pump fillage, increasing efficiency

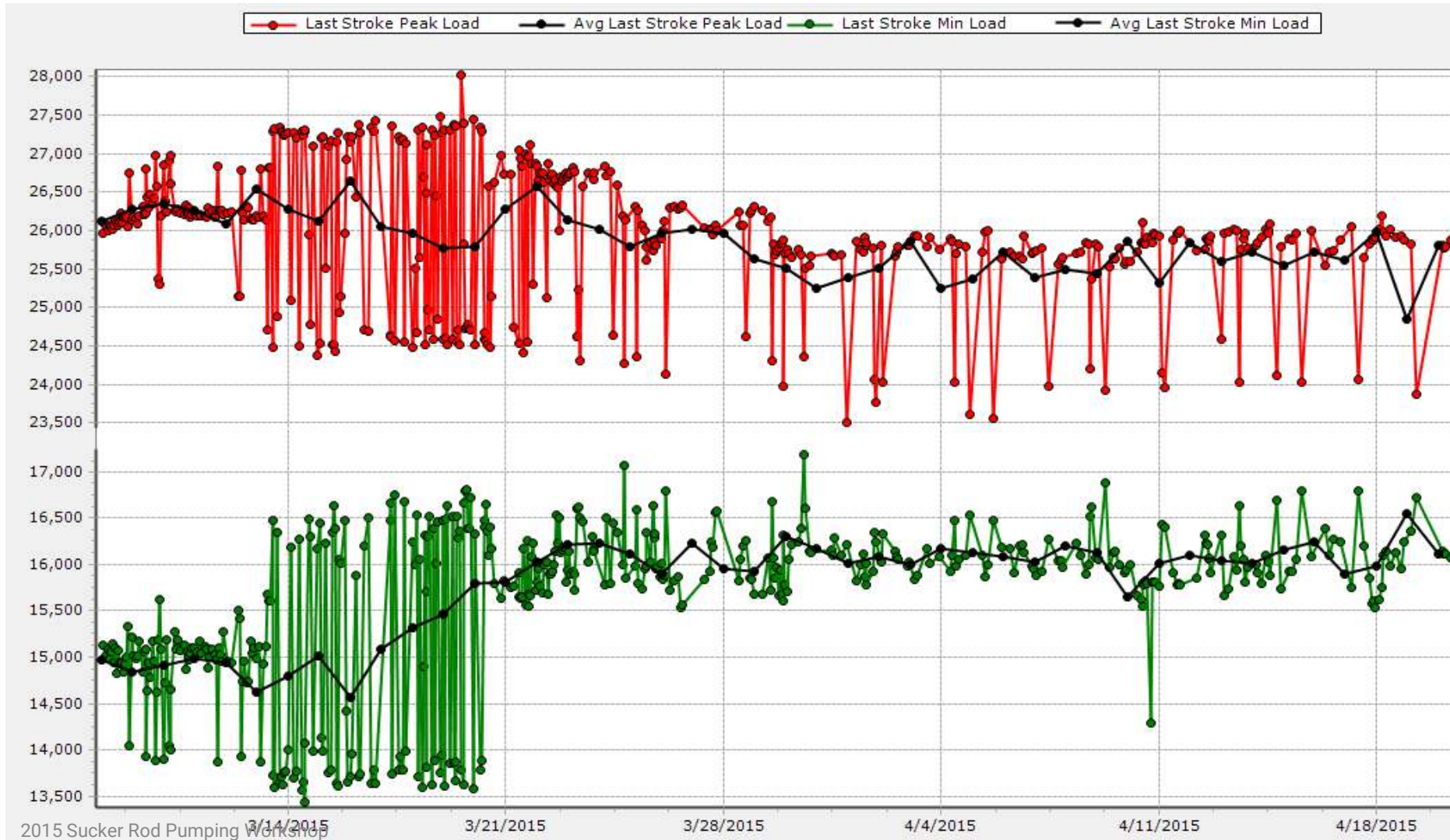
- ▶ Also more time for evolving gas to exit gas anchor
  - ▶ Less gas enters pump, more liquid
- ▶ Higher minimum rod loads due to slow downstroke/ less gas
  - ▶ Reduces buckling tendencies
  - ▶ Allows higher maximum rod loads
- ▶ **Has nothing to do with setting pumping speeds**
  - ▶ That is PSO Part 2

# Well #1: 35% reduction in strokes per day, oil production not significantly affected





# Well #1: Minimum load increased by 1000 pounds, maximum load same



2015 Sucker Rod Pumping Workshop



## Why PSO Part 2 works

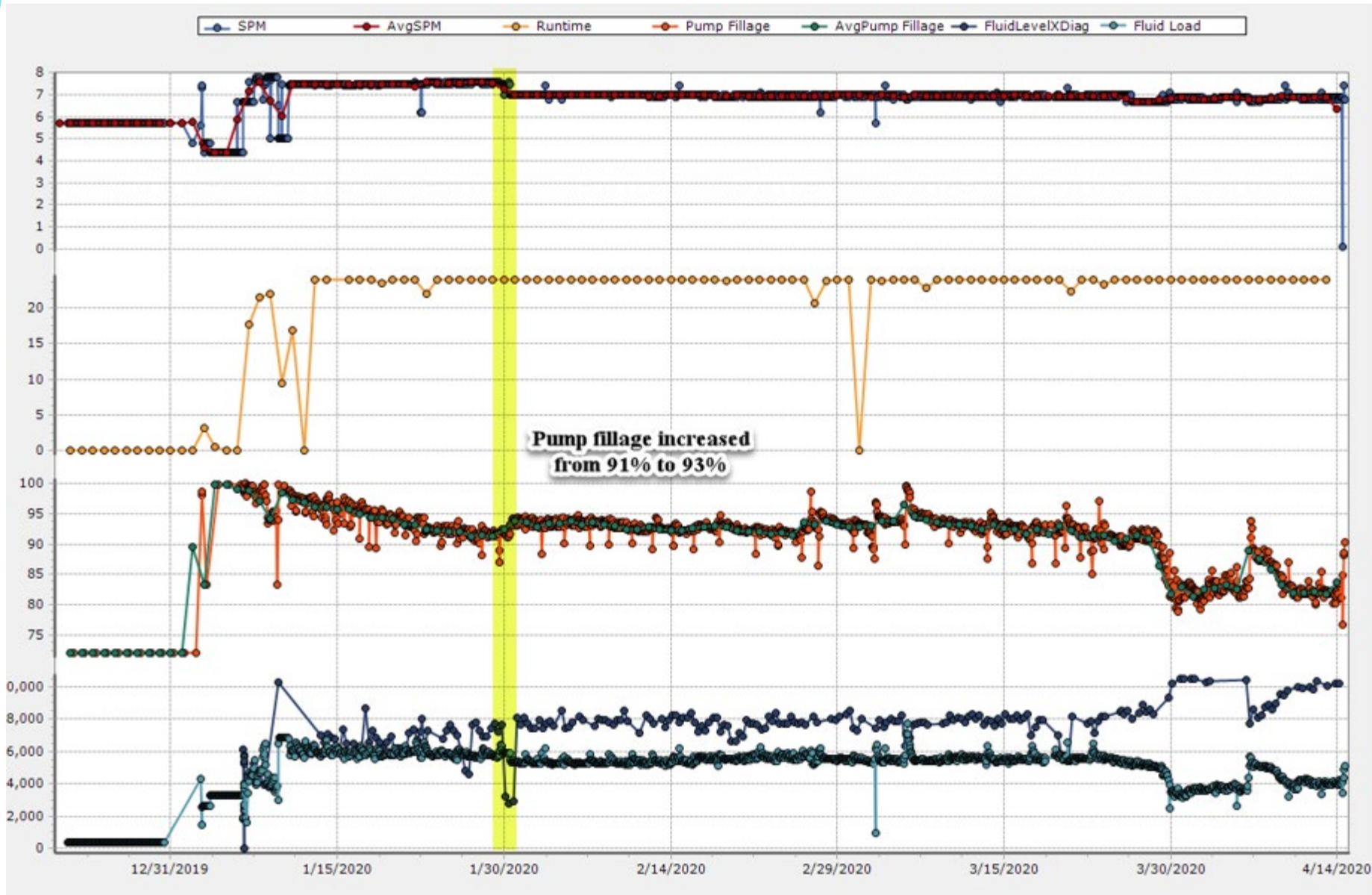
- ▶ PSO Part 2 does what you would do, create maximum working speed setpoints that are better aligned with the average production rate
- ▶ This prevents over-reacting to high pump fillages often seen at the beginning of a slug event
- ▶ Keeping the maximum pumping speed slightly higher than average pumping speed helps avoid low pump fillage events and rod buckling

# Some operators are using SDSM today



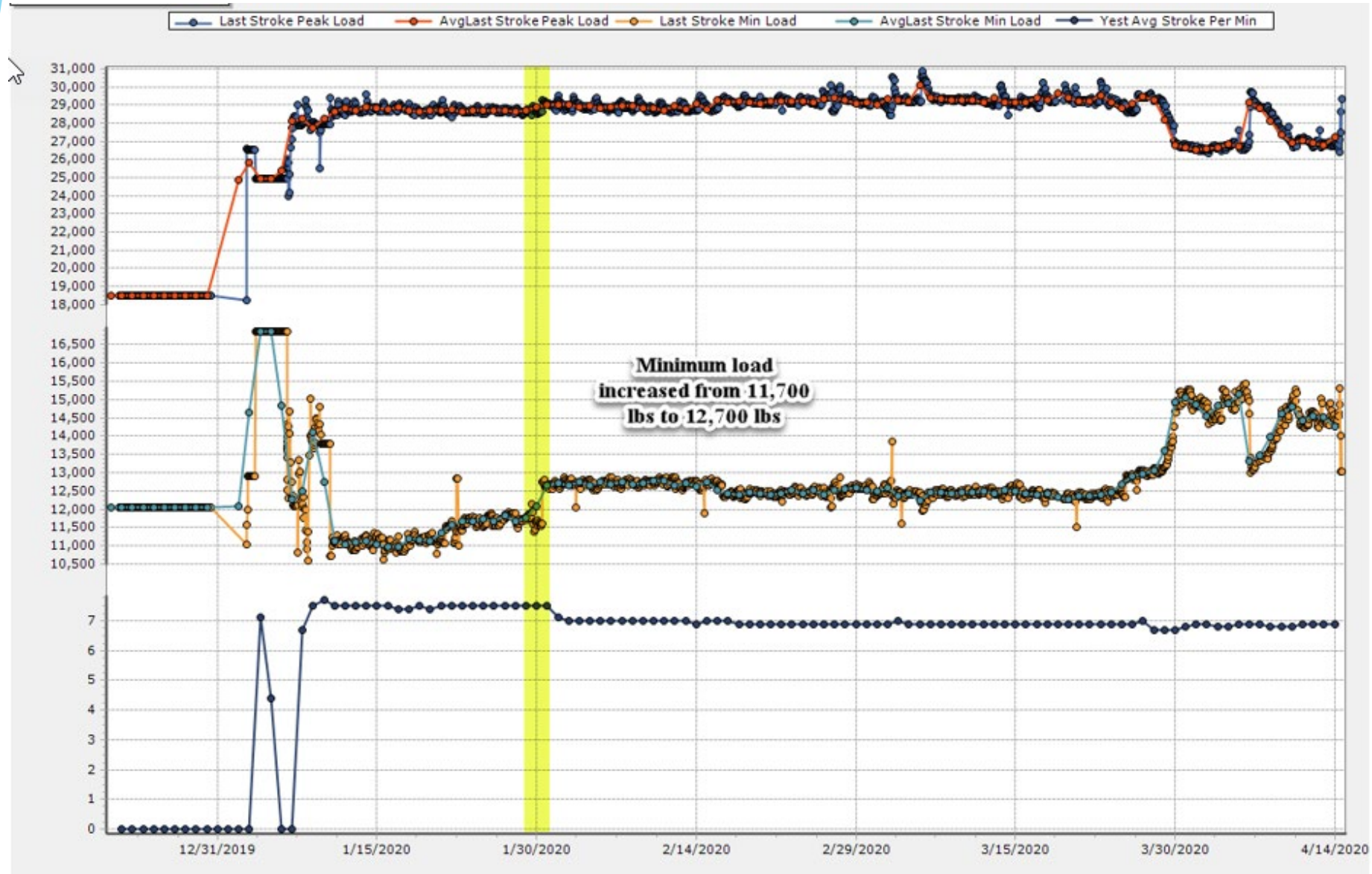
- ▶ Continental Resources using SDSM in Bakken
  - ▶ No hardware modifications needed
  - ▶ Using Scada to load SDSM settings into RPC's
- ▶ Operator in Eagle Ford using SDSM on 400+ wells
  - ▶ Working towards applying PSO Part 2 via Data Analytics

# Continental Resources SDSM Results

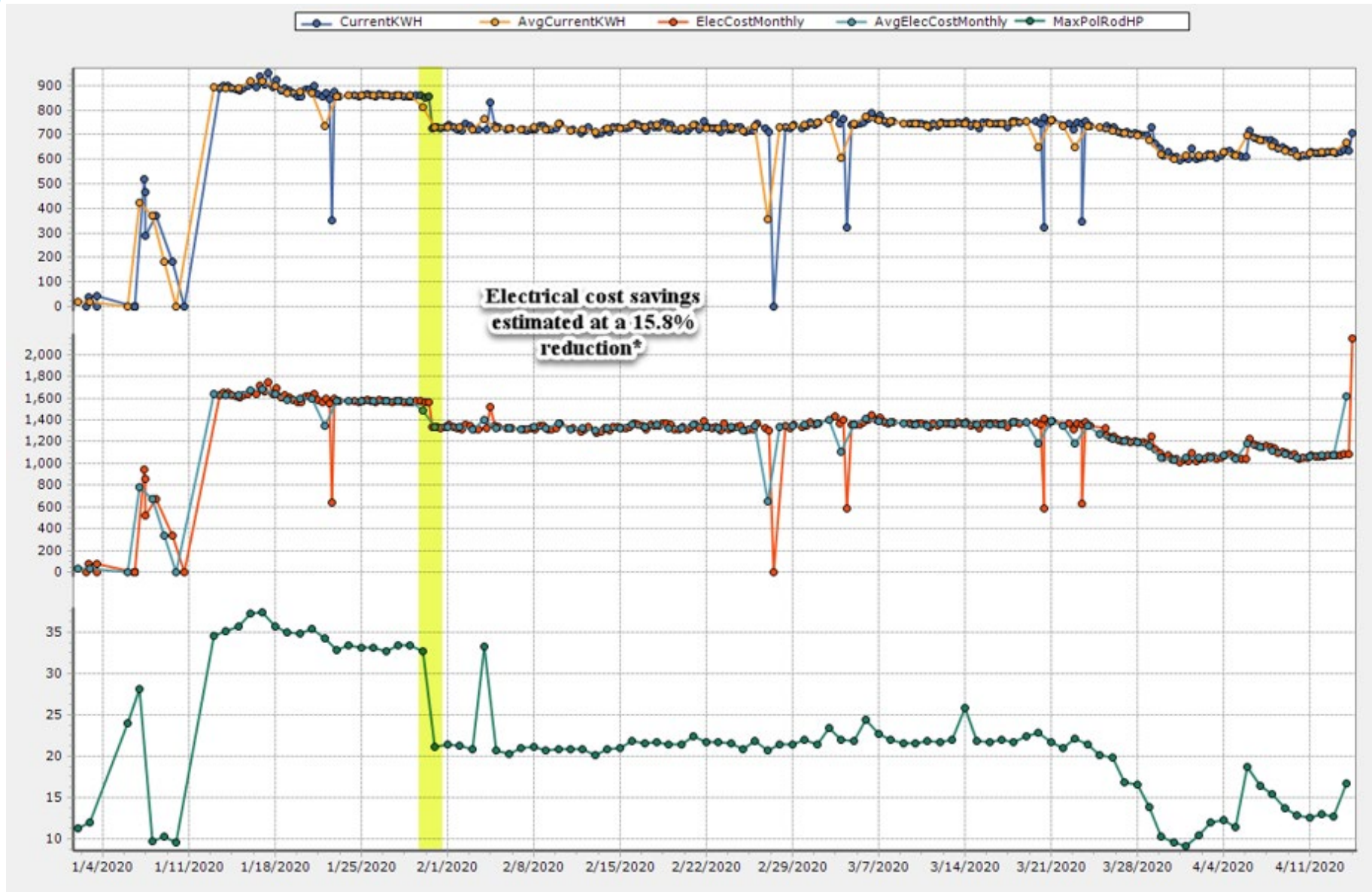




# Continental Resources SDSM Results



# Continental Resources SDSM Results





# Continental Resources SDSM Results



# Factors Working Against PSO Adoption



- ▶ SDSM / PSO doesn't increase production
  - ▶ Makes same production with less strokes (less wear)
  - ▶ Lower power consumption documented
  - ▶ Neither were home run reasons
- ▶ Could not prove that less strokes and higher minimum rod loads would result in less failures
  - ▶ No long-term failure studies performed
- ▶ Pumps with leaking standing valves lost production
  - ▶ 5% of pilot test wells saw this

# Factors Working Against PSO Adoption

- ▶ Is major change in operation
  - ▶ Simulation programs can't handle it
  - ▶ Unrealized fears about equipment failures
  - ▶ Required PLC to be inserted in RPC cabinet
- ▶ RPC companies felt threatened
  - ▶ Wasn't invented by them
  - ▶ Hardware could not perform PSO Part 2
  - ▶ Encline had applied for a patent
  - ▶ Result: Warranty voided if operator tried
- ▶ Oil price dropped and spending stopped



# Factors Working Against PSO Adoption



# Factors Working Against PSO Adoption



- ▶ Gas Lift became popular for horizontals
  - ▶ Less industry interest in rod pumping
  - ▶ Introduction of HPGL in 2016 shifted Encline resources from PSO due to idea importance
- ▶ Slow Downstroke Mode and PSO are not plug and play
  - ▶ SDSM requires routine parameter review
  - ▶ PSO sets all parameters, but requires periodic algorithm evaluation
  - ▶ Neither simple enough for busy operator personnel
  - ▶ Opportunities for Machine Learning?



# The Future?

- ▶ Encline dropped all patent efforts years ago when it became clear that adoption would be difficult
- ▶ RPC manufacturers are free to incorporate PSO
- ▶ Operators are free to incorporate PSO into Data Analytics / Machine Learning efforts
  - ▶ Let the cloud tell the RPC upstroke and downstroke pumping speeds
- ▶ Encline has free guide to SDSM setup. Visit [enclinelift.com](http://enclinelift.com) and request in contact section





# Acknowledgements/Thanks & Questions

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Thanks to all operators who performed trials of PSO and opted to support Encline's R&D efforts by purchasing PSO hardware



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